

# A-103S

## Macroporous Weak Base Anion Exchange Resin

(For the demineralization of sugar solutions)

### Technical Data

#### PRODUCT DESCRIPTION

**Purolite A-103S** is a macroporous poly (vinylbenzyl) tertiary amine exchanger of moderate porosity, specially developed for use in the demineralization of juices from the beet, cane and liquid sugar industries. Its (relatively high) basicity permits adsorption of organic acids of pKa values up to about 5, and its macroporous structure results in excellent resistance to both osmotic shock and organic fouling. As a result, many of the high molecular weight color bodies present are also removed, (in beet sugar juices, the reduction in color may be 80% or more), and these color bodies can readily be eluted during the regeneration. This can be carried out with low

amounts of caustic soda, ammonia, or soda ash to give high operating capacities. The resin, with its macroporous styrene-divinylbenzene matrix, not only possesses good rinse characteristics, but its high total exchange capacity ensures high ash-removal figures (often >75% of total), with significant savings in running cost thanks to its excellent regeneration efficiency.

Where both the ionic concentration and color are particularly high in the influent juice, the more porous version of this resin, **Purolite A-100S**, is recommended as an alternative.

Typical Physical & Chemical Characteristics	
Polymer Matrix Structure	Macroporous Styrene-divinylbenzene
Physical Form and Appearance	Opaque near-white spherical beads
Whole Bead Count	95% min.
Functional Groups	Tertiary amino
Ionic Form, as shipped	Free base
Shipping Weight (approx.)	650 g/l (41 lb/ft <sup>3</sup> )
Screen Size Range: - U.S. Standard Screen	16 - 40 mesh, wet
Particle Size Range	+1.2 mm <2%, -0.42 mm <2%
Moisture Retention, FB form,	40 - 45%
Cl <sup>-</sup> form,	48 - 55%
Reversible Swelling FB → Cl <sup>-</sup>	25% max.
Specific Gravity, moist FB Form	1.04
moist Cl <sup>-</sup> Form	1.06
Total Exchange Capacity, Cl <sup>-</sup> form,	
wet, volumetric	1.6 meq/ml min.
dry, weight	4.1 meq/g min.
Strong Base %	12 - 20
Operating Temperature, Cl <sup>-</sup> Form	100°C (212°F) max.
pH Range, Stability	0 - 14
pH Range, Operating	0 - 8

## HYDRAULIC CHARACTERISTICS

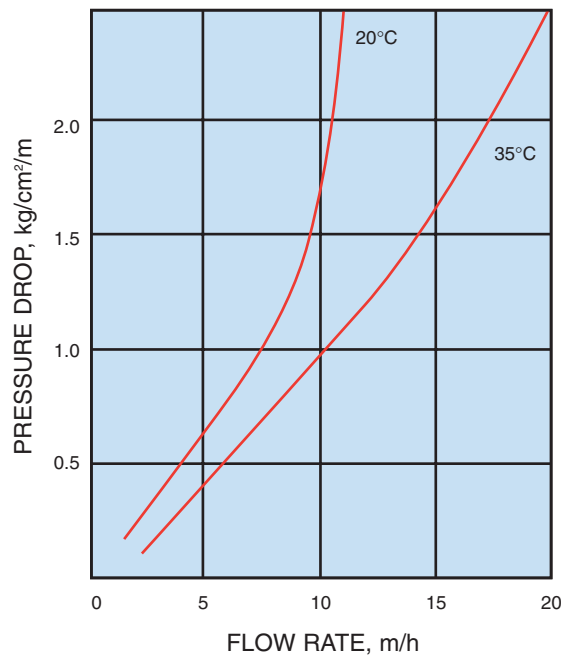
The pressure drop (headloss) across a properly classified bed of ion-exchange resin depends on the particle size distribution, bed depth, and void volume of the exchanger, and on the flowrate and viscosity (and hence on the temperature) of the influent solution. Anything affecting any of these parameters, for example the presence of particulate matter filtered out by the bed, abnormal compaction of the resin bed, or the incomplete classification of the resin spheres will have an adverse effect, and result in an increased headloss.

Pressure drop figures obtained on thin sugar juice, at 12°Brix and temperatures of 20°C, (68°F), and 35°C, (95°F), correspond to those for 5°C and 20°C respec-

tively in water itself, and are given in the graph below for **Purolite A-103S**.

During upflow backwash, the resin bed should be expanded in volume by 50%, in order to free it from any particulate matter in the influent solution, to clear the bed of bubbles and voids, and to reclassify the resin particles as much as possible, ensuring minimum resistance to flow. Since both viscosities and densities of the influent in special applications systems will vary quite widely, backwash expansion figures are not given here, but for dilute aqueous solutions the expansion as a function of flowrate is essentially similar to that of **Purolite A-103S** on backwash after rinse with demineralized water.

**PRESSURE DROP IN 12°BRIX THIN JUICE**



Conversion of Units	
1 m/h (cubic meters per square meter per hour)	= 0.341 gpm/ft <sup>2</sup> = 0.409 U.S. gpm/ft <sup>2</sup>
1 kg/cm <sup>2</sup> /m (kilograms per square cm per meter of bed)	= 4.33 psi/ft = 1.03 atmos/m = 10 ft H <sub>2</sub> O/ft

## CHEMICAL STABILITY

**Purolite A-103S** is insoluble in acids, alkalis, and all common solvents. Most salt forms and the free base are stable at elevated temperatures, and may be used in continuous service at temperatures up to about 90°C (ca. 195°F) without significant change occurring. However,

exposure to free chlorine, and certain oxidizing agents such as peroxides may lead to loss in exchange capacity as the result of ongoing chemical reaction, and should therefore be avoided.

## APPLICATIONS TO SUCROSE

The principal sources of sucrose are sugar cane and sugar beet, which are crushed or shredded respectively before extraction with hot water to obtain the impure sugar juice. The first purification step on this juice is the removal of both soluble and colloidal impurities by the addition of lime, followed by precipitation of the calcium as calcium carbonate by carbonation with CO<sub>2</sub>. After filtration, and cooling to minimize sucrose breakdown catalyzed by H<sup>+</sup> ions from the cation exchanger, the thin juice at a concentration of 10 - 15°Brix may be demineralized using a strong-acid cation exchanger, **Purolite C100S**, followed by a weak-base anion resin such as **Purolite A-103S** or **Purolite A-100S**. The elimination of the residual Ca<sup>++</sup> ions and much of the residual color results in increased yields of higher purity sugar at

the crystallization stage. With liquid sugar solutions, where no additional purification on crystallization can take place, effective demineralization and decolorization are essential for high-purity products.

Regeneration of a **Purolite A-103S** (or **A-100S**) unit is normally carried out with 2% caustic soda at about 4 bed volumes (b.v.) per hour, after a 1.5 b.v. "sweetening off" and backwashing. Following a rinse with water, and "sweetening on" with a further 1.5 b.v. of the thin decationized juice, the unit is ready to recommence service. The run is monitored by conductivity and color, and a lifetime of approximately 1000 cycles may be expected (depending on the characteristics of the juice being treated) before performance is seriously affected.

## APPLICATIONS TO OTHER SUGARS

**Purolite A-103S** may also be used in the demineralization of high-solids glucose liquors, or HFCS (high fructose corn syrups), where a strongbase anion resin cannot be used in the OH<sup>-</sup> form because of color formation by the so-called Maillard reaction. Regeneration with 5% soda ash, or better 2.5% ammonia, will minimize OH<sup>-</sup> formation on the small amount of quaternary groups which may be present. Ammonia is preferred because of its lower cost, ease of recovery, and the lower rinse

requirements accompanying its use. Since the influent solutions are, in general, relatively high viscosity liquids (a 50°Brix solution at about 30°C has a viscosity of about 10 cp.), the temperatures used are higher than with the thin juices to obtain suitable flow rates. The macroporous structure of **Purolite A-103S** is designed to resist both the osmotic and thermal shocks arising from this mode of operation.

## OTHER APPLICATIONS

Deionization of sorbitol solutions is carried out in essentially the same way as for solutions of sugar. The efficient removal of formic acid from quite concentrated solutions of formaldehyde at temperatures up to 60 - 65°C can be achieved, provided that multivalent

cations of iron and other transition metals are absent. Operating capacities of 45 - 50g HCOOH per l of resin (2.8 - 3.0 lb./ft<sup>3</sup>) have been recorded, depending on the influent temperature, concentration, and the regeneration level of the exchanger.

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